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# Distribution coefficients of *n*-alkanes measured on wall-coated capillary columns

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## Abstract

Distribution coefficients K of *n*-alkanes were determined in wide ranges of temperature and carbon numbers from gas chromatographic retention data measured on wall-coated poly(dimethylsiloxane) commercial capillary columns. A discussion is centered on how to mitigate the difficulties for an accurate determination of K when using weakly retentive columns, as those bearing very high phase ratios or short lengths. Particularly, the errors associated with the estimation of the gas hold-up and the phase ratio of the column are considered. The chromatographic importance for determining K of *n*-alkanes relies on the fact that these are the most commonly applied references for reporting relative thermodynamic parameters such as the Kovats Index and the relative retention. A great amount of information has been compiled in this form. If K of the reference is known, absolute values of distribution coefficients for a myriad of substances are readily obtainable. The knowledge of K(T) functions of solutes in wide ranges of temperature is a primary necessity in temperature-programmed gas chromatography. This knowledge is needed for the prediction of absolute retention times and for computing separation optimizations of mixtures containing several critical pairs of analytes. © 2000 Elsevier Science BV. All rights reserved.

Keywords: Distribution coefficients; Capillary columns; Thermodynamic parameters; Alkanes

## 1. Introduction

At the thermodynamic equilibrium, the solvation of a solute in the bulk solvent is quantified by the logarithm of solute molecule's numeral density ratio in both phases [1,2]:

$$\ln\left(\frac{{}^{\mathrm{L}}\rho_2}{{}^{\mathrm{G}}\rho_2}\right)_{\mathrm{eq}} = \ln K_{\mathrm{L}} = -\frac{\Delta G^*}{kT}$$
(1)

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*E-mail address:* rex@dalton.quimica.unlp.edu.ar (F.R González) The number density ratio of solute molecules in the liquid and gas solutions,  ${}^{L}\rho_{2}/{}^{G}\rho_{2}$ , is equal to the gas-liquid distribution coefficient  $K_{\rm L}$ . The pseudochemical potential difference  $\Delta G^{*}$  is the average Gibbs free energy for the process of transferring one solute molecule from the ideal gas into a fixed position in the bulk liquid solution. This is a statistical ensemble average over all possible configurations of molecules around the solute and possible conformations of solute and solvent [1].

Since  $\ln K_{\rm L}$  is the relevant thermodynamic quantity of solvation, it must be the parameter to be compared between systems when the bulk solution is the principal occurring process. The purpose of the

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present article is to report and compare chromatographically determined related values, that we shall denote ln K. The studied system is n-alkane solutes in poly(dimethylsiloxane) (PDMS) solvent. This study is realized employing commercial wall-coated capillary columns with different lengths and phase ratios, in order to cover a wide range of temperatures and chain lengths of the solutes. The value of  $K_{\rm I}$  of present interest is that involving ideal behavior of the gas phase and infinite dilution. That is to say, it must be ensured that the interactions in the gas phase are negligible. The solute should mainly interact with the liquid stationary phase, with [solute-solute] and [solute-dissolved carrier gas] interactions in this phase also being negligible. The applied pressures and the injected quantity into the column must correspond to these conditions.

Beside its intrinsic physicochemical importance, the function  $K_{I}(T)$  of *n*-alkanes in the studied solvent holds a particular chromatographic relevance. This homologous series of solutes was the most widely applied reference system for the determination of relative thermodynamic parameters such as the Kovats Index and the relative retention. A great amount of information has been compiled under these forms [3,4]. For translating this information into absolute values of  $K_{I}$ , the distribution coefficient of the reference ought to be known. Determining the  $K_{I}(T)$  functions of solutes in wide range of temperatures is a primary chromatographic need. In temperature-programmed gas chromatography (TPGC), it enables the numerical prediction of absolute retention times and the performance of computational optimizations for the separation of mixtures containing several critical pairs of analytes (see e.g., Ref. [5] and the references cited therein).

Notwithstanding the great advantages of silicone capillary columns, there is scarce published information on  $K_L$ , covering the wide *T* intervals applied in current analysis. This fact is originated in diverse experimental difficulties inherent to the determination of absolute  $K_L$  from chromatographic retention data (see e.g., Ref. [6]). One basic objective of the present paper is to discuss and illustrate how these difficulties can be circumvented. Firstly, we shall introduce a brief review of these difficulties.

The ratio of liquid phase volume to interfacial area (as e.g., the gas-liquid interfacial area) for wall-

coated capillary columns has the order  $V_{\rm L}/A_{\rm i} \cong d_{\rm f} \sim$  $10^{-5}$  cm, where  $d_{\rm f}$  is the average film thickness of stationary phase coating in the column. This value is comparably very low with respect to that of a solution contained in a small vessel, which has an order  $V_{\rm L}/A_{\rm i} \sim 1$  cm. The latter is the order of  $V_{\rm L}/A_{\rm i}$ met by other methods for determining  $K_{\rm L}$ , as for example in the Ben Naim–Baer instrument [7–9]. If the solute-solvent molecular forces of interaction greatly differ from the solvent-solvent ones, the accumulation of solute in the inter-phase region, or either its depletion with respect to the bulk liquid concentration, may occur. This is the consequence of, either, the decrease or increase in the solution's interfacial free energy per unit area (viz. the surface tension) due to the presence of the solute [10]. The system evolves to the least total free energy, and the concentration of solute in this region will evolve accordingly. Therefore, we should be aware that the incidence of interfacial phenomena might be significant in capillary gas-liquid chromatography [11-14]. In the particular case of the system we study in the present paper, it is expected that the chromatographically measured K will not depend on  $V_{\rm L}$  $A_i \cong d_f$ , namely, the interfacial effect should be negligible. Another possible reason for the dependence of the chromatographic K on  $d_{\rm f}$  is the existence of a slow mass transfer leading to non-equilibrium conditions [6], but this effect is not expected considering the thin  $d_{\rm f}$  for coatings of capillary columns.

The equation of isothermal retention, in the absence of interfacial and extra-column effects, is:

$$t_{\rm R} = t_{\rm M} (1 + K_{\rm L} \beta^{-1}) \tag{2}$$

 $t_{\rm R}$  is the retention time,  $\beta$  is the volume ratio of gas and liquid phases,  $\beta = V_{\rm G}/V_{\rm L}$ , and  $t_{\rm M}$  is the gas hold-up. The latter is the retention time of a nonretained solute, a solute with  $K_{\rm L}=0$ . This is a hypothetical solute that cannot permeate into the liquid phase. All real molecules used as  $t_{\rm M}$  markers actually permeate the polymers usually employed as stationary phases [15], and in some cases the fusedsilica capillary wall [16].

Eq. (2) assumes that the position of the chromatographic peak is defined by its maximum. This condition is solely valid for perfectly symmetrical peaks. The position of an asymmetric peak is defined by  $t_1$ , the first moment of its time-distribution function [6]. The peaks eluting from very short capillary columns are generally skewed.

As is stated in Eq. (2), the determination of  $K_{\rm L}$  from chromatographic retention data demands the precise knowledge of  $t_{\rm M}$  and  $\beta$ . The difficulties associated with the accurate determination of these two basic chromatographic parameters are, respectively, the central topics of Sections 3 and 4.

## 2. Experimental

Three columns were employed in this study. These are described in Table 1. The specifications in the table are nominal values reported by the manufacturer. The column identified as column 1 presents a high retention. This is a long column, bearing a length, L = 50 m, with a relatively low nominal phase ratio,  $\beta = 151$ . This column allows one to determine K of alkanes with a low carbon number n. Column 2 has the same specifications but it is very short, having an L of only 12 m. Column 3 has a very high nominal phase ratio,  $\beta = 800$ , with a very thin film. Columns 2 and 3 admit measuring the retention of alkanes with higher carbon numbers, n, up to 32. All measurements were run in a Hewlett-Packard 5880A chromatograph. Flame ionization detection was used in all cases. The applied split ratios ranged from 60

to 100:1, using hydrogen as the carrier gas. The retention times,  $t_{\rm R}$ , were measured with a precision of 0.001 min. The injected quantities were such that, invariably, the recorded peak areas were lower than 1000 counts, and in the same order for all the *n*-alkanes eluted in the same chromatogram. In the employed instrument one count approximately corresponds to one detected picocoulomb. As a guideline, the response of combined detector-integrator is 5000 pC/ $\mu$ l of injected methane (1  $\mu$ l~0.65  $\mu$ g of methane at ambient p and T). The approximate upper limit of 1000 counts was found for not detecting any variation in the last digit of  $t_{\rm R}$  due to the injected amount of sample. For column 1, the ratio of absolute inlet/outlet pressures was systematically varied from  $P \equiv p_i/p_o = 1.4$  to 2.6. The outlet pressure  $p_0$  was the atmospheric pressure. The variation of pressures was done with a dual aim. First, to detect any dynamic effect owing to masstransport phenomena, i.e., a dependence of the chromatographic K on the linear velocity u of carrier gas. Second, to either detect any thermodynamic effect as the pressure dependence of K caused by non-ideal behavior of the gas phase [6]. For columns 2 and 3 the range of P was 1.3-1.6. The oven temperature was monitored with three calibrated chromel-constantan thermocouples connected to a digital instrument (Omega Engineering, Stanford, CT, USA). These were located in an equilateral triangle array near to the column coil. Reported

Table 1

| Columns employed | l in | this | work | for | the | determination | of | K | of | n-alkanes | a |
|------------------|------|------|------|-----|-----|---------------|----|---|----|-----------|---|
|------------------|------|------|------|-----|-----|---------------|----|---|----|-----------|---|

| 1      |                            |  |            |   |
|--------|----------------------------|--|------------|---|
| Column | Commercial name            | Specifications (nominal values)                                  | etanominal | $\beta$ calculated regression to Eq. (10) |
| 1      | HP-1<br>(crosslinked PDMS) | L = 50  m<br>$d_c = 200 \mu\text{m}$<br>$d_f = 0.33 \mu\text{m}$ | 151        | 160.4                                     |
| 2      | HP-1<br>(crosslinked PDMS) | L = 12  m<br>$d_c = 200 \mu\text{m}$<br>$d_r = 0.33 \mu\text{m}$ | 151        | 157.8                                     |
| 3      | SPB-1<br>(bonded PDMS)     | L = 30  m<br>$d_c = 320 \mu\text{m}$<br>$d_f = 0.10 \mu\text{m}$ | 800        | 850.6                                     |

<sup>a</sup> Column length, *L*; column internal diameter,  $d_c$ ; coating film thickness,  $d_f$ . The column nominal phase ratio is  $\beta = d_c/4d_f$ . The calculated  $\beta$  is the average of four values obtained by regression of  $t_R(n)$  data to Eq. (10), involving four different chromatograms in the range T = 120 to  $220^{\circ}$ C. The lowest possible *n* were applied (see Tables 3–4 and Section 4).

temperatures have an error of  $\pm 1^{\circ}$ C. Temperature gradients across the oven were such that a difference of less than 1°C was detected between thermocouples for  $T < 200^{\circ}$ C, greater gradients were found for the higher temperature range.

Multi-parametric non-linear regressions of *n*-alkane isothermal retention data  $t_{\rm R}(n)$  were performed with commercial software (Sigma Plot, Jandel Scientific, CA, USA). This applies the algorithm of Marquardt.

### 3. On the determination of gas hold-up

The correct determination of the parameter  $t_{\rm M}$  has been a controversial issue since the initiation of GC [17–26]. Great confusion in the literature has originated in the relationship between its physical significance and those experimental entities that may be correlative [26]. Three general approaches for  $t_{\rm M}$ determination have been described: (a) calculation by fluid mechanics; (b) calculation through the retention of markers supposedly being completely insoluble, i.e., assuming that the marker's  $t_{\rm R}$  would practically coincide with  $t_{\rm M}$ ; (c) calculation through multiparametric regression of isothermal  $t_{\rm R}(n)$  data of homologous series, as e.g., the *n*-alkanes.

Approach (a) is based upon the application of basic relationships from fluid mechanics. The expression of  $t_{\rm M}$  is obtained by integration of the differential form of Hagen–Poiseulle's equation, leading to [27]:

$$t_{\rm M} = \frac{128\eta}{3p_{\rm o}} \cdot \left(\frac{L}{d_{\rm c}}\right)^2 \cdot \left[\frac{P^3 - 1}{\left(P^2 - 1\right)^2}\right]$$
(3)

This, or the equivalent expression in terms of flow-rates, will not permit an accurate determination of  $t_{\rm M}$  due to the intrinsic errors of measurement in the average internal column diameter  $d_{\rm c}$ , the gas viscosity  $\eta$ , or the flow-rate. Experimental results show that even when  $d_{\rm c}$  is specified by electronic microscopy, considerable discrepancy of results is computed between flow-rate [28] and pressure [25] measurements. Excessively high values of  $t_{\rm M}$ , close to  $t_{\rm R}$  of methane, have been reported by this method [25].

Method (b) cannot be applied since all gases used

as  $t_{\rm M}$  markers permeate the PDMS polymer, and therefore, are invariably retained to some extent [15].

Method (c) is based on the property of  $\ln K_{\rm L}$  (or  $-\Delta G^*/kT$ ), for homologous series such as the *n*-alkanes, of being a smoothly increasing function of the carbon number *n* when  $n \ge 5$ . This assertion is valid under constant chromatographic conditions. According to Eqs. (1) and (2), in isothermal and perfectly constant conditions, and in the absence of interfacial effects, the retention time of any *n*-alkane is given by:

$$t_{\rm R}(n) = t_{\rm M} + \frac{t_{\rm M}}{\beta} \cdot \exp\left[\frac{-\Delta G^*(n)}{kT}\right] \quad (\text{const. } p, T)$$
(4)

If a functional form is provided for  $\Delta G^*(n)$ , the corresponding multi-parametric regression of experimental  $t_{\rm R}(n)$  data will render the values for the parameters of the equation, i.e.,  $t_{\rm M}$  and the parameters contained in the second term of the right hand side. Function  $-\Delta G^*(n)/kT$ , viz. In  $K_{\rm L}(n)$ , very slightly deviates from linearity [29]. In consequence, any appropriate empirical non-linear expression contained in the exponential of Eq. (4) will accurately represent the experimental behavior of  $t_{\rm R}(n)$ , yielding the correct calculated value of  $t_{\rm M}$ . A theoretical expression of  $\Delta G^*(n)$  has been derived from elementary concepts of statistical thermodynamics [2], leading to:

$$t_{\rm R}(n) = t_{\rm M} + \exp \left[ A + B(n-2) + \ln \left( 1 - Cn^2 \right) \right]$$
(5)

In this, or in any empirical expression [21,23,24], the exponential term gains importance at increasing n, becoming relatively less important as the contribution to  $t_R(n)$  from the first term  $t_M$ . Hence, in the determination of the parameter  $t_M$  by curve fitting, the statistical weights for  $t_R$  values of low n are more significant. When a low retention column is used, like those with a great phase ratio or a short length, the smaller n-alkanes cannot be included in the chromatogram. Consequently, the determination of  $t_M$  by the n-alkane regression method loses exactitude. Another reason for the lack of reliability of the calculated  $t_M$  in these types of columns is their lower magnitudes, introducing greater percentage

Table 2 Short column 2<sup>a</sup>

| <i>T</i> (°C) | п  | $t_{\rm R}(n) \exp((min))$ | $t_{\rm R}(n)$ calc. <sup>b</sup><br>(min) | Parameters obtained by regression to Eq. (5) | $t_{\rm M}$ calculated from $t_{\rm R}$ and $K_{\rm L}$ of methane Eq. (8) | $t_{\rm R}$ of methane (exp.) |
|---------------|----|----------------------------|--|--|--|-------------------------------|
| 280           | 20 | 1.434                      | 1.434                                      | $t_{\rm M} = 0.875 \pm 0.0014$               | 0.879  | 0.885                         |
|               | 22 | 1.762                      | 1.762                                      | $A = -4.842 \pm 0.0094$                      |  |                               |
|               | 24 | 2.280                      | 2.280                                      | $B = 0.242 \pm 0.0005$                       |  |                               |
|               | 26 | 3.094                      | 3.094                                      | $C = 0.00024 \pm 0.000005$                   |  |                               |
|               | 30 | 6.354                      | 6.354                                      |  |  |                               |
|               | 32 | 9.439                      | 9.439                                      |  |  |                               |
| 300           | 20 | 1.067                      | 1.067                                      | $t_{\rm M} = 0.763 \pm 0.0026$               | 0.758  | 0.763                         |
|               | 22 | 1.228                      | 1.228                                      | $A = -5.097 \pm 0.031$                       |  |                               |
|               | 24 | 1.470                      | 1.470                                      | $B = 0.223 \pm 0.0017$                       |  |                               |
|               | 26 | 1.834                      | 1.835                                      | $C = 0.00025 \pm 0.000015$                   |  |                               |
|               | 28 | 2.382                      | 2.382                                      |  |  |                               |
|               | 30 | 3.200                      | 3.200                                      |  |  |                               |
|               | 32 | 4.415                      | 4.415                                      |  |  |                               |

<sup>a</sup> Due to the application of excessively high *n*, two anomalous values of  $t_{\rm M}$  are obtained by the *n*-alkanes regression method. These are compared with  $t_{\rm M}$  calculated from the retention of methane and its  $K_{\rm L}$ . At 280°C the  $t_{\rm M}$  obtained by regression is too low. At 300°C the inverse situation is attained;  $t_{\rm M}$  obtained by regression is equal to  $t_{\rm R}$  of methane, thus exceeding the expected value.

 ${}^{b} t_{R}(n)$  calc. values are calculated with the parameters of the regression. The applied software uses 15 characters for the calculations. In all tables the parameters are rounded to 3 or 4 digits for an easier comparison.

standard errors. In order to illustrate this situation, Table 2 indicates the retention times used in the regressions and the calculated parameters for the short column 2. These only include values of n > 20, which are excessively high for an accurate determination of  $t_{\rm M}$ , particularly considering the errors originated by peak asymmetry in this column. Strictly,  $t_{\rm R}$  should be replaced by  $t_1$  in Eqs. (2) or (4). In one case the calculated  $t_{\rm M}$  is excessively low compared to  $t_{\rm M}$  derived from the retention of methane and its  $K_{\rm L}$ . On the other case the calculated  $t_{\rm M}$  is equal to the retention of methane, a condition that has no physical sense [26]. These two chromatograms were unique examples where significant deviations were detected, but are illustrative of what could occur in principle in other cases.

The described regression method for  $t_{\rm M}$  determination is only applicable when the retention times of the shorter *n*-alkanes are included in the chromatogram, i.e., for long columns having a reduced phase ratio, in the order  $\beta \sim 100$ . This situation demands seeking another way of estimating  $t_{\rm M}$  in weakly retentive columns, especially for the short columns where peak asymmetry is important. To overcome this difficulty, one possibility is to use a  $t_{\rm M}$  marker whose K(T) function has been previously established

through adequate experimental conditions. We shall employ here the ln K(T) function of methane reported in a preceding publication [29]. This was determined in the 50 m column with nominal  $\beta$  = 151. Although for a more accurate determination of K of methane a column of at least 100 m with  $\beta$ ~100 would be needed at temperatures between 80 and 120°C, the lack of data from the current literature covering this issue compels us to adopt K(T)reported in Ref. [29]<sup>1</sup>. The behavior in the range 40–120°C is described by the following polynomial of the reciprocal absolute temperature:

$$\ln K(CH_4) = 1.401 - 2106(1/T) + 616 \ 275(1/T)^2$$

$$(313 \le T \le 393 \text{ K}) \tag{6}$$

For the practical purpose of determining  $t_{\rm M}$ , the behavior at temperatures over 120°C may be approximated to [26]:

$$K(CH_4) \cong 1 \quad (T \ge 393 \text{ K}) \tag{7}$$

<sup>&</sup>lt;sup>1</sup>More accurate determinations of methane's  $K_{\rm L}$  near ambient temperature should be obtained by using other methods, rather than GC, such as measuring it in the Ben Naim–Baer apparatus.

By using the relationships given by Eqs.(6) and (7),  $t_{\rm M}$  can then be estimated through Eq. (2):

$$t_{\rm M} = t_{\rm R}({\rm CH}_4) \cdot \frac{\beta}{\beta + K({\rm CH}_4)} \tag{8}$$

When the retention times are measured with a precision of 0.001 min, it can be checked easily that for  $K \sim 1$  and  $\beta > 250$ , variations of almost 10% in  $\beta$ do not induce any change in the last digit of the calculated  $t_{\rm M}$ . Therefore, nominal values of  $\beta$  can be used in Eq. (8) as a first approximation, provided this  $\beta$  will be corrected a posteriori applying some appropriate estimation of the parameter.

The latter described procedure is the one employed for determining  $t_{\rm M}$  in the chromatograms of columns 2 and 3. The regression to Eq. (5) was the method employed for column 1, and this generated the reported  $K(CH_{4})$  function.

## Table 3

| Column 2      | a  |                           |  |   |  |                               |
|---------------|----|---------------------------|--|---|--|-------------------------------|
| <i>T</i> (°C) | n  | $t_{\rm R}(n)$ exp. (min) | $t_{\rm R}(n)$ calc. <sup>b</sup><br>(min) | Parameters obtained by regression to Eq. (10) | $t_{\rm M}$ calculated from $t_{\rm R}$ and $K_{\rm L}$ of methane Eq. (8) | $t_{\rm R}$ of methane (exp.) |
| 120           | 9  | 0.871                     | 0.871                                      | $\beta = 157.6 \pm 0.8$                       | 0.525  | 0.528                         |
|               | 10 | 1.137                     | 1.137                                      | $B = 0.593 \pm 0.0010$                        |  |                               |
|               | 11 | 1.604                     | 1.604                                      | $C = 0.00111 \pm 0.00003$                     |  |                               |
|               | 12 | 2.420                     | 2.420                                      |   |  |                               |
| 200           | 14 | 1.392                     | 1.390                                      | $\beta = 156.8 \pm 1.9$                       | 0.792  | 0.797                         |
|               | 16 | 2.020                     | 2.023                                      | $B = 0.373 \pm 0.0010$                        |  |                               |
|               | 20 | 5.938                     | 5.937                                      | $C = 0.000378 \pm 0.000015$                   |  |                               |
|               | 22 | 11.237                    | 11.238                                     |   |  |                               |
|               | 24 | 21.887                    | 21.887                                     |   |  |                               |
| 220           | 12 | 1.003                     | 1.003                                      | $\beta = 157.7 \pm 1.2$                       | 0.906  | 0.912                         |
|               | 13 | 1.079                     | 1.079                                      | $B = 0.337 \pm 0.0008$                        |  |                               |
|               | 14 | 1.182                     | 1.183                                      | $C = 0.000390 \pm 0.000013$                   |  |                               |
|               | 16 | 1.526                     | 1.526                                      |   |  |                               |
|               | 18 | 2.175                     | 2.175                                      |   |  |                               |
|               | 20 | 3.397                     | 3.397                                      |   |  |                               |
|               | 22 | 5.689                     | 5.689                                      |   |  |                               |
| 220           | 18 | 1.755                     | 1.757                                      | $\beta = 159.0 \pm 2.2$                       | 0.653  | 0.657                         |
|               | 20 | 2.746                     | 2.744                                      | $B = 0.337 \pm 0.001$                         |  |                               |
|               | 22 | 4.592                     | 4.592                                      | $C = 0.00040 \pm 0.000012$                    |  |                               |
|               | 24 | 8.027                     | 8.028                                      |   |  |                               |
|               | 26 | 14.367                    | 14.367                                     |   |  |                               |

<sup>a</sup> Estimation of  $\beta$  by curve fitting to Eq. (10), using  $t_{\rm M}$  calculated from the retention of methane and its  $K_{\rm L}$ .

 ${}^{b} t_{R}(n)$  calc. values are calculated with the parameters of the regression and  $t_{M}$  reported in the sixth column. The latter is a constant for the curve fit to Eq. (10). The applied software uses 15 characters for the calculations. In all tables the parameters are rounded to 3 or 4 digits for an easier comparison.

## 4. On the determination of the phase ratio

In the current method the volume ratio of gas to liquid phases can be guessed through the information on the column's construction. From this information the geometric parameters of the column may be estimated roughly. For wall-coated capillary columns the phase ratio can be approximated to:

$$\beta \equiv \frac{V_{\rm G}}{V_{\rm L}} \cong \frac{d_{\rm c}}{4d_{\rm f}} \tag{9}$$

Great difficulties for a direct accurate determination of the average column internal diameter  $d_c$ and film thickness  $d_{\rm f}$  are evident. Usually,  $d_{\rm f}$  is estimated indirectly through information from the coating method [30-34]. When the dynamic method is utilized, the film thickness is a function of the passage velocity of the solution containing the stationary phase. A perfectly uniform film thickness

along the whole column length cannot be assured [30]. Therefore, in these estimations of the parameters great uncertainty is attained, even when the time consuming static method of coating is applied [30].

In Ref. [29] was shown that for the retention of *n*-alkanes on PDMS at temperatures over  $120^{\circ}$ C, the contribution to  $\Delta G^{*}(n)/kT$  independent of *n* becomes negligible. This absent contribution is ascribed to end methyl C–H bonds. With this condition, Eq. (4) is reduced to:

$$t_{\rm R}(n) = t_{\rm M} + \frac{t_{\rm M}}{\beta} \cdot \exp\left[B(n-1) + \ln\left(1 - Cn^2\right)\right]$$
(10)

Table 4

where (n-1) is the number of C–C bonds in the alkane molecule. If  $t_{\rm M}$  is determined by other means than curve fitting, as e.g., using methane as the marker and its previously determined K(T) function, the unknown parameters are  $\beta$ , *B* and *C*. Hence, the *n*-alkane regression method can now be applied for calculating only  $\beta$ , *B* and *C*.

Tables 3 and 4 show the results obtained by the regressions of  $t_{\rm R}(n)$  data to Eq. (10), respectively, in columns 2 and 3. Temperatures are between 120 and 220°C. The chromatograms containing the lowest *n* possible were included (recalling that *n* must be  $\geq 5$ ). The gas hold-up is not a parameter to be determined; it is a constant in the curve fitting

| Column :      | 5  |                           |  |   |  |   |
|---------------|----|---------------------------|--|---|--|---|
| <i>T</i> (°C) | п  | $t_{\rm R}(n)$ exp. (min) | $t_{\rm R}(n)$ calc. <sup>b</sup><br>(min) | Parameters obtained by regression to Eq. (10) | $t_{\rm M}$ calculated from $t_{\rm R}$ and $K_{\rm L}$ of methane Eq. (8) | <i>t</i> <sub>R</sub> of methane (exp.) |
| 120           | 8  | 1.669                     | 1.669                                      | $\beta = 849.8 \pm 7.2$                       | 1.561  | 1.563                                   |
|               | 9  | 1.753                     | 1.753                                      | $B = 0.591 \pm 0.0014$                        |  |   |
|               | 10 | 1.900                     | 1.900                                      | $C = 0.000998 \pm 0.000039$                   |  |   |
|               | 11 | 2.159                     | 2.159                                      |   |  |   |
|               | 12 | 2.614                     | 2.614                                      |   |  |   |
|               | 14 | 4.789                     | 4.789                                      |   |  |   |
| 140           | 8  | 1.686                     | 1.687                                      | $\beta = 852.5 \pm 5.1$                       | 1.616  | 1.618                                   |
|               | 9  | 1.734                     | 1.734                                      | $B = 0.524 \pm 0.0007$                        |  |   |
|               | 10 | 1.812                     | 1.812                                      | $C = 0.000738 \pm 0.000014$                   |  |   |
|               | 11 | 1.942                     | 1.942                                      |   |  |   |
|               | 12 | 2.156                     | 2.156                                      |   |  |   |
|               | 13 | 2.511                     | 2.510                                      |   |  |   |
|               | 14 | 3.090                     | 3.091                                      |   |  |   |
|               | 16 | 5.605                     | 5.605                                      |   |  |   |
|               | 18 | 12.290                    | 12.290                                     |   |  |   |
| 160           | 8  | 1.723                     | 1.723                                      | $\beta = 850.0 \pm 5.4$                       | 1.673  | 1.675                                   |
|               | 9  | 1.751                     | 1.751                                      | $B = 0.467 \pm 0.00076$                       |  |   |
|               | 10 | 1.796                     | 1.796                                      | $C = 0.000610 \pm 0.000016$                   |  |   |
|               | 11 | 1.867                     | 1.867                                      |   |  |   |
|               | 13 | 2.152                     | 2.152                                      |   |  |   |
|               | 14 | 2.423                     | 2.423                                      |   |  |   |
|               | 16 | 3.501                     | 3.501                                      |   |  |   |
|               | 18 | 6.096                     | 6.096                                      |   |  |   |
| 180           | 12 | 1.915                     | 1.915                                      | $\beta = 850.3 \pm 3.4$                       | 1.730  | 1.732                                   |
|               | 13 | 2.008                     | 2.008                                      | $B = 0.418 \pm 0.0014$                        |  |   |
|               | 14 | 2.145                     | 2.145                                      | $C = 0.000518 \pm 0.000015$                   |  |   |
|               | 16 | 2.656                     | 2.656                                      |   |  |   |
|               | 18 | 3.779                     | 3.779                                      |   |  |   |
| a — .         |    |                           |  |   |  |   |

<sup>a</sup> Estimation of  $\beta$  by curve fitting to Eq. (10), using  $t_{\rm M}$  calculated from the retention of methane and its  $K_{\rm L}$ .

 ${}^{b} t_{R}(n)$  calc. values are calculated with the parameters of the regression and  $t_{M}$  reported in the sixth column. The latter is a constant for the curve fit to Eq. (10). The applied software uses 15 characters for the calculations. In all tables the parameters are rounded to 3 or 4 digits for an easier comparison.

| Tablı<br>Ln <i>K</i> | s 5<br>tabulé | ated as     | s func        | tion of            | Т               |        |              |                |         |               |               |                |              |               |               |               |                |               |               |               |               |          |                 |          |         |              |                |               |
|----------------------|---------------|-------------|---------------|--------------------|-----------------|--------|--------------|----------------|---------|---------------|---------------|----------------|--------------|---------------|---------------|---------------|----------------|---------------|---------------|---------------|---------------|----------|-----------------|----------|---------|--------------|----------------|---------------|
| T (°C)               | Ln K          |             |               |                    |                 |        |              |                |         |               |               |                |              |               |               |               |                |               |               |               |               |          |                 |          |         |              |                |               |
|                      | n = 6         |             |               | n = 7              |                 | = u    | 8            |                | = u     | 6=            |               | n = 1          | 0            |               | n = 11        |               |                | <i>n</i> =12  |               |               | <i>n</i> = 13 |          | 1               | ı=14     |         | = <i>u</i>   | - 16           |               |
|                      | Column<br>1   | column<br>2 | n Column<br>3 | a Column Co<br>1 2 | olumn Coli<br>3 | umn Cc | olumn C<br>2 | olumn Col<br>3 | lumn Cc | olumn Cc<br>2 | olumn Cc<br>3 | lumn Colu<br>1 | mn Colu<br>2 | mn Colur<br>3 | mn Colun<br>1 | an Colur<br>2 | ın Colum.<br>3 | n Columi<br>1 | 1 Column<br>2 | 1 Column<br>3 | Column<br>1   | Column 2 | Column (<br>3 1 | Column C | olumn C | Column Cc    | humn Colt<br>2 | ımn Colt<br>3 |
| 40                   | 4.979         |             |               | 5.900              | 5.88            | 32 6.5 | 815          | 6.75           | 94 7.7  | 724           | L.T.          | 02             |              |               |               |               |                |               |               |               |               |          |                 |          |         |              |                |               |
| 50                   | 4.646         | 4.64        |               | 5.510 5            | 501             | 9.5    | 372 6.       | 363            | 7.2     | 229 7.2       | 220           |                |              |               |               |               |                |               |               |               |               |          |                 |          |         |              |                |               |
| 60                   | 4.338         |             | 4.324         | 5.155              | 5.13            | 38 5.5 | 967 5.       | 953 5.9:       | 50 6.7  | 775 6.5       | 757 6.7       | 56 7.57.       | 3 7.557      | 7.558         |               | 8.359         |                |               |               | 9.152         |               |          | 9.938           |          |         |              |                |               |
| 70                   | 4.059         |             |               | 4.825 4.           | 81              | 5.5    | 593 5.       | 576            | 6.3     | 353 6.2       | 339           | 7.11:          | 2 7.098      | ~~            |               | 7.852         |                |               | 8.604         |               |               |          |                 |          |         |              |                |               |
| 80                   | 3.794         |             | 3.768         | 4.520              | 4.49            | 94 5.2 | 241 5.       | 224 5.2        | 23 5.5  | 096           | 5.5           | 41 6.67.       | 5 6.655      | 6.655         | 7.390         | 7.368         | 7.367          |               | 8.077         | 8.074         |               | -        | 8.779           |          |         |              |                |               |
| 90                   | 3.560         |             |               | 4.244              |                 | 4.5    | 924          |                | 5.6     | 502           |               | 6.27           | 2            |               |               |               |                |               |               |               |               |          |                 |          |         |              |                |               |
| 100                  | 3.330         |             |               | 3.976              | 3.96            | 50 4.t | 621          | 4.6            | 07 5.2  | 261 5.2       | 243 5.2       | 45 5.89        | 8 5.882      | 5.883         | 6.533         | 6.514         | 6.516          | 7.166         | 7.145         | 7.147         |               |          | 7.774           |          | 8       | 1,404        |                | 9.64          |
| 120                  | 2.926         |             |               | 3.509              | 3.50            | )1 4.( | 083          | 4.0            | 73 4.6  | 561 4.t       | 55 4.6        | 48 5.23        | 9 5.217      | 5.217         | 5.800         | 5.782         | 5.786          | 6.364         | 6.346         | 6.350         |               | -        | 6.912           |          | 7       | .472         |                | 8.58          |
| 140                  | 2.587         |             |               | 3.107              |                 | 3.t    | 620          | 3.6            | 13 4.1  | i.4 137       | 12 4.1        | 24 4.64        | 5 4.64       | 4.635         | 5.154         | 5.142         | 5.144          | 5.661         | 5.647         | 5.650         |               | -        | 6.155 (         | 5.660    | 9       | .654         |                | 7.65          |
| 160                  | 2.305         |             |               | 2.764              |                 | 3.2    | 229          | 3.2            | 36 3.£  | 576 3.(       | 58 3.f        | 80 4.13        | 8 4.13       | 4.136         | 4.594         | 4.58          | 4.591          | 5.051         | 5.038         | 5.039         | 5.494         | -        | 5.494 5         | 5.949 5. | 945 5   | .942         | 6.83           | 9 6.83        |
| 180                  | 2.052         |             |               | 2.464              |                 | 2.5    | 878          |                | 3.2     | 288 3.2       | 56            | 3.69.          | 4            |               | 4.104         | 4.10          |                | 4.511         | 4.51          | 4.515         | 4.920         | -        | 4.918 5         | 5.322    | 5       | 1318         |                | 6.12          |
| 200                  | 1.809         |             |               | 2.188              |                 | 2.5    | 580          |                | 2.5     | 355           |               | 3.30           | ~            |               | 3.689         |               |                | 4.043         |               | 4.035         |               | 4.37     | 4.378 4         | 4.778    | 4       | <i>LTT</i> . | 5.50           | 0 5.49        |
| 220                  | 1.617         |             |               | 1.939              |                 | 2.2    | 262          |                | 2.6     | 513           |               | 2.95.          | 2            |               | 3.291         |               |                | 3.624         |               |               |               | 3.97     | 4               | 1.283 4. | 287     |              | 4.94           | 0             |
| 240                  |               |             |               | 1.756              |                 |        |              |                | 2.5     | 364           |               |                |              |               |               |               |                |               |               |               |               |          |                 | 3.       | 88      |              | 4.45           | 3 4.44        |
| Į                    |               |             |               |                    |                 |        |              |                |         |               |               |                |              |               |               |               |                |               |               |               |               |          |                 |          |         |              |                |               |

| <i>T</i> (°C) | Ln K            |                 |                 |                 |                 |                 |                 |                 |
|---------------|-----------------|-----------------|-----------------|-----------------|-----------------|-----------------|-----------------|-----------------|
|               | n=18            | n=20            | n=22            | n=24            | n=26            | n=28            | n=30            | n=32            |
| 140           | 8.633, column 3 |                 |                 |                 |                 |                 |                 |                 |
| 160           | 7.721, column 2 |                 |                 |                 |                 |                 |                 |                 |
|               | 7.718, column 3 |                 |                 |                 |                 |                 |                 |                 |
| 180           | 6.917, column 3 |                 |                 |                 |                 |                 |                 |                 |
| 200           | 6.180, column 3 | 6.933, column 2 | 7.641, column 3 | 8.344, column 3 |                 |                 |                 |                 |
| 220           | 5.587, column 2 | 6.226, column 2 | 6.860, column 2 | 7.489, column 2 | 8.111, column 2 |                 |                 |                 |
| 240           | 5.049, column 2 | 5.621, column 2 | 6.192, column 2 | 6.752, column 2 | 7.322, column 2 | 7.864, column 2 | 8.421, column2  |                 |
|               | 5.051, column 3 |                 |                 |                 |                 | 7.853, column 3 | 8.436, column 3 |                 |
| 260           |                 | 5.081, column 2 | 5.594, column 2 | 6.105, column 2 | 6.611, column 2 | 7.113, column 2 | 7.611, column 2 | 8.103, column 2 |
| 280           |                 | 4.596, column 2 | 5.060, column 2 | 5.522, column 2 | 5.981, column 2 | 6.432, column 2 | 6.886, column 2 | 7.332, column 2 |
| 300           |                 | 4.209, column 2 | 4.618, column 2 | 5.026, column 2 | 5.434, column 2 | 5.843, column 2 | 6.249, column 2 | 6.651, column 2 |

Table 6 Measured ln K of *n*-alkanes in the range of chain lengths from n = 18 to 32

calculation. The employed  $t_{\rm M}$  are reported in the sixth column of these tables. In Ref. [29]  $\beta$  and  $t_{\rm M}$  were simultaneously determined for column 1 by the regression method.

The same consideration, as described in the preceding section, is applicable to the determination of  $\beta$  by regression. If the exponential factor of Eq. (10) is excessively high, great standard errors on the calculated  $\beta$  will be attained. Therefore, it is advisable that an adequate range of *n* should be included in the chromatogram. This means that chromatograms obtained at temperatures greater than 200°C should not be considered in the case of columns 2 and 3.

The average value of  $\beta$  from the reported four curve fits in Tables 3 and 4 are shown in the last column of Table 1. The comparison of the nominal and calculated  $\beta$  reveals discrepancies of about 6% for columns 1 and 3, while the difference is lower for column 2, though this was produced by the same manufacturer of column 1.

## 5. Results and discussion

Tables 5 and 6 reports values of ln *K* as function of *T* for each solute. At a given temperature, *K* was calculated from the retention time  $t_{\rm R}$  of the solute according to:

$$K = \left(\frac{t_{\rm R}}{t_{\rm M}} - 1\right) \cdot \beta \tag{11}$$

As was mentioned in Section 3,  $t_{\rm M}$  in columns 2 and 3 was determined through Eq. (8) using the  $t_{\rm R}$  of methane, its reported K(T) and  $\beta$  reported in the last column of Table 1. In most cases methane could be injected in the same chromatogram. When the sample contained higher homologues, the presence of solvent deprived us from injecting the marker in the same chromatogram owing to lack of resolution of marker and solvent. In these cases methane was injected alone immediately previous or posterior to the sample chromatogram.

Through the systematic variation of the head pressure in column 1, from P=1.4 to 2.6, no significant changes were detected on the measured ln *K* beyond the experimental error. Table 7 illustrates this observation through representative examples.

| Table 7  |       |    |      |          |    |           |           |    |        |
|----------|-------|----|------|----------|----|-----------|-----------|----|--------|
| Examples | of ln | Kd | lata | measured | at | different | pressures | in | column |
| 1ª _     |       |    |      |          |    |           | -         |    |        |

| T (°C) | Р   | Measured ln K | Average | Standard deviation |
|--------|-----|---------------|---------|--------------------|
| 60     | 1.4 | 4.342         | 4.338   | 0.003              |
|        | 1.7 | 4.333         |         |                    |
|        | 1.8 | 4.343         |         |                    |
|        | 1.9 | 4.341         |         |                    |
|        | 2.0 | 4.336         |         |                    |
|        | 2.1 | 4.336         |         |                    |
|        | 2.2 | 4.337         |         |                    |
|        | 2.6 | 4.339         |         |                    |
| 80     | 1.4 | 3.797         | 3.794   | 0.005              |
|        | 1.7 | 3.786         |         |                    |
|        | 1.8 | 3.798         |         |                    |
|        | 1.9 | 3.797         |         |                    |
|        | 2.6 | 3.790         |         |                    |
| 100    | 1.4 | 3.329         | 3.330   | 0.006              |
|        | 1.8 | 3.335         |         |                    |
|        | 2.0 | 3.335         |         |                    |
|        | 2.2 | 3.323         |         |                    |
|        | 2.2 | 3.333         |         |                    |
|        | 2.6 | 3.323         |         |                    |
| 120    | 1.4 | 2.933         | 2.926   | 0.008              |
|        | 1.7 | 2.916         |         |                    |
|        | 1.8 | 2.933         |         |                    |
|        | 2.4 | 2.920         |         |                    |
|        | 2.6 | 2.928         |         |                    |

<sup>a</sup> The reported data belong to n=6.

Differences between runs present random fluctuations that reveal the precision of measurement in the employed chromatograph, not a systematic effect of pressure on K. Therefore, in the context of the present accuracy of measurement, ideal behavior of the gas phase can be assumed in the applied pressure interval. The average of measured ln K at different P, are the values reported in Table 5 for column 1. The reported ln K for columns 2 and 3 are also the average of different measurements, in many cases. Generally, the dispersion increases when T is incremented, as can be observed in the column of standard deviations of Table 7. The increasing temperature gradients in the oven, and the consequent reduction of temperature control, is the cause of this expected result.

From n = 8 to 12 the solutes could be measured in all three columns in relatively wide *T* intervals, without greatly differing intrinsic errors, i.e., without

too extreme differences in the orders of measured ratios  $t_{\rm R}/t_{\rm M}$ . This allows the comparison between columns. It can be seen in Table 5 that there are no discrepancies between columns 2 and 3, greater than the experimental dispersion. Since there is a threefold relation in their  $d_{\rm f}$ , interfacial effects can also be assumed to be negligible. The discrepancies between column 1 and the others fluctuate around 0.3–0.6% at temperatures below 140°C. In principle, this could be ascribed to the greater errors in the determination of  $\beta$  for this column, considering that four parameters were determined by the regressions, not three as in the other cases. But the discrepancies vanish at temperatures over 140°C. Both columns 1 and 2 belong to the same manufacturer, even though, differences in the cross-linking of the polymer may occur, considering that this process is carried out in situ. A difference in the composition might be the origin for the discrepancy [35].

Fig. 1 represents  $\ln K$  as a function of the number of C–C bonds at high temperatures. The purpose of these plots is to illustrate graphically the increasing dispersion generated by incrementing *T*, and the application of different chromatograms and columns. This can be compared with the same graph in Ref. [29]. Therein, data from the same chromatogram



Fig. 1. Experimental ln K plotted as function of the number of C–C bonds. The same symbols are used for data obtained in different chromatograms and columns. The filled line is the theoretical expression  $\ln K = B(n-1) + \ln (1-Cn^2)$ . Dispersion increases dramatically with temperature due to the temperature gradients in the oven of the chromatograph.

were plotted in each curve at lower temperatures, so no dispersion could be observed graphically, and even numerically.

The theoretical physical interpretation that originated the construction of Fig. 1 in Ref. [29] is that at temperatures over 120°C C–H bonds should not contribute significantly to  $-\Delta G^*(n)/kT$ , and consequently, the existing contributions arise mainly from C–C bonds. This hypothesis derives from the observation on the experimental behavior of K(T) of methane and the correspondent physical interpretation [26,29]. Therefore, when the number of C–C bonds in the *n*-alkane molecule tends to zero ln *K* should tend to be negligible.

## 6. Conclusions

Ln *K* of *n*-alkanes were measured in wide range of temperatures and carbon numbers. Commercial PDMS capillary columns with phase ratios in almost both extremes of current use were employed. The phase ratios were determined by regression. No important differences in ln *K* between columns were found. No pressure effect on ln *K* was observed using hydrogen as the carrier gas. This fact indicates that ideal behavior of the mobile phase can be assumed within the chromatographic error for pressures up to almost 3 bar (abs.). The interfacial effect was not detectable, since the film thickness had no influence on *K*. Therefore, we may presume that the informed ln *K* corresponds to ln  $K_1$ .

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